

Solution of the Heat and Mass Transfer Problem for Soil Radiant Heating Conditions Using the Method of Finite Integral Fourier Transform

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Abstract. To achieve high agricultural yields, it is essential to predict the soil temperature and moisture regime, considering the heating technology employed. The research object is soil heated by a ceiling-mounted infrared emitter. The research subject encompasses one-dimensional unsteady fields of soil moisture content and temperature. The research goal is to forecast the soil temperature and moisture regime under radiant heating conditions. The research methods involve the analytical solution of heat and mass transfer differential equations using the method of finite integral Fourier transforms. Research results indicate that the top layer of milled peat, with an initial moisture content of 3.7 kg/kg, will reach a final moisture content of 1.0 kg/kg in approximately 6 hours during infrared drying. As a result of radiant heating, the soil temperature will rise from an initial 5 °C to a final 22.6 °C in approximately 3 hours. The analytical solution of the mass transfer differential equation can be utilized for theoretical studies of drying capillary-porous materials, such as determining the drying period or the thickness of the material layer that will dry to a specified final moisture content. The analytical solution of the heat transfer differential equation,

accounting for both thermal conductivity and the Dufour effect, can be employed to manage the operation of the infrared radiation source, such as determining its operational and shutdown periods when the soil surface temperature reaches its maximum (critical) value. The mathematical solutions discussed in the article do not consider thermodiffusion processes in the soil layer (Soret effect), which presents a promising direction for further scientific research.

Keywords: Moisture Content, Temperature, Heat and Mass Transfer Differential Equations; One-Dimensional Unsteady Field, Soil, Radiant Heating, Dufour Effect, Soret Effect.

1 Introduction

Research on thermal and mass transfer processes occurring in cultivation structures, such as greenhouses designed for year-round plant cultivation, can be conducted at various hierarchical levels [1–5]. On one hand, in the development of software and engineering methods for designing and calculating heating systems, it is essential to consider the thermal and material balances of the entire facility where agricultural crops (e.g., tomatoes, cucumbers) are grown, including its enclosure and soil surface (integral approach) [6–10]. This approach necessitates accounting for the interconnection of heat and mass flows and their impact on the microclimate parameters within the facility: the temperature and relative humidity of the indoor air, and the soil surface temperature. On the other hand, there is scientific interest in a differential approach, where heat and mass transfer are studied locally within an individual element of the greenhouse, rather than in the entire greenhouse as a whole [11, 12]. From the perspective of favorable plant growth, development, and fruiting, it is evident that this element is the soil, where the desired variables may be moisture content and temperature of the layer, varying with coordinates and time.

As is well known, research on various heat and mass transfer processes occurring in physical bodies [13–15] is associated with solving problems of molecular energy and substance transport, which typically follow linear laws (e.g., heat conduction is described by Fourier's linear law). These linear laws form the basis for deriving the corresponding differential equations. Solving these equations under specific initial and boundary conditions, which characterize the initial state of the body and its surface interactions with the surrounding environment, presents well-known mathematical challenges [16–21]. Since the late 18th century, mathematicians from different countries have developed various methods for solving heat and mass transfer differential equations. Through the development of experimental methods, a direct relationship between energy and substance transport processes has been established (e.g., thermal energy transport can occur not only due to thermal conductivity but also due to concentration differences in a mixture, concentration gradient – Dufour effect) [22–30]. This is also characteristic of soil, which is a colloidal capillary-porous body, particularly under conditions of radiant heating [31–33].

Research object: soil heated by a ceiling-mounted infrared emitter.

Research subject: one-dimensional unsteady fields of soil moisture content and temperature.

Research objective: to predict the soil temperature and moisture regime under radiant heating conditions.

Research tasks:

1. Formulation of the problem. Establishment of boundary conditions corresponding to the radiant heating of the soil surface.

2. Obtaining solutions to the heat and mass transfer differential equations using the method of finite integral Fourier transforms.
3. Examination of the analytical solution of the heat and mass transfer differential equations in a specific example.
4. Description of the obtained solution results.

2 Methodology

Formulation of the mass transfer problem. Consider a soil layer of infinite dimensions along the coordinate axes $0x$ and $0y$ (Figure 1), with a characteristic linear dimension along the $0z$ – thickness L , m. The initial moisture content of the soil layer (at time $t = 0$) along the coordinate interval $z \in [0; L]$ is known and equals W_0 , kg/kg. Due to radiant heating, moisture evaporates from the soil surface into the surrounding environment at a constant rate j , kg/(m² · s), resulting in a change in soil moisture content along the $0z$ coordinate over time t , s. Determine the moisture content distribution $W(z, t)$.

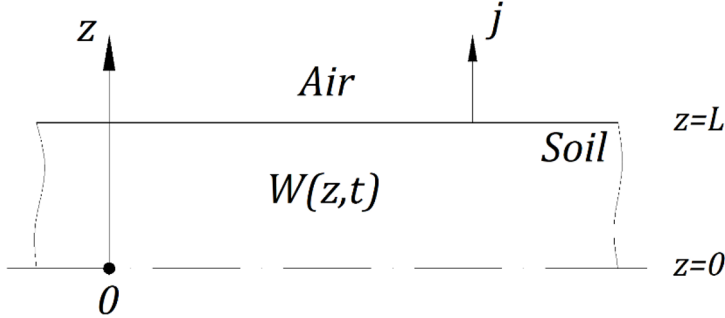


Fig. 1. Formulation of the mass transfer problem.

In radiant heating, the evaporation rate at the soil surface can be determined using Dalton's formula:

$$j = \alpha_m (p_{surf} - p_{\infty}), \text{ kg/(m}^2 \cdot \text{s)}, \quad (1)$$

where α_m is the external moisture exchange coefficient (mass transfer coefficient), kg/(m² · s · Pa), which is calculated using criterion similarity equations for mass transfer processes or approximated by Lewis's formula; p_{surf} and p_{∞} are the partial vapor pressures at the soil surface and in the ambient environment, respectively, Pa.

The differential mass transfer equation and the boundary conditions for its solution are as follows (Figure 1):

$$\frac{\partial W(z,t)}{\partial t} = D \frac{\partial^2 W(z,t)}{\partial z^2} \quad (0 \leq z \leq L, t > 0), \quad (2)$$

$$W(z, 0) = W_0, \quad (3)$$

$$D\rho \frac{\partial W(L,t)}{\partial z} + j = 0, \quad (4)$$

$$W(0, t) = W_0, \quad \frac{\partial W(0,t)}{\partial z} = 0, \quad (5)$$

where W is the moisture content, kg/kg; z is the coordinate, m; t is time, s; D is the soil diffusion coefficient, m²/s; ρ is the soil density, kg/m³; j is the evaporation rate at the soil surface, kg/(m² · s).

The solution to the mass transfer differential equation (2) with initial (3) and boundary (4), (5) conditions is known and is given by:

$$\begin{aligned}
W(z, t) = & W_0 - \frac{jL}{D\rho} \left[\text{Fo}_W - \frac{1}{6} \left(1 - 3 \frac{z^2}{L^2} \right) + \right. \\
& + \sum_{n=1}^{\infty} (-1)^{n+1} \frac{2}{n^2 \pi^2} \cos \left(n \pi \frac{z}{L} \right) e^{-n^2 \pi^2 \text{Fo}_W} + \\
& \left. + \frac{2W_0}{L^2} \sum_{n=1}^{\infty} \cos \left(n \pi \frac{z}{L} \right) e^{-n^2 \pi^2 \text{Fo}_W} \cdot \int_0^h \cos \left(n \pi \frac{z}{L} \right) dz \right],
\end{aligned} \quad (6)$$

where $\text{Fo}_W = \frac{Dt}{L^2}$ this is the Fourier number for mass transfer.

Formulation of the heat transfer problem. Consider a soil layer of infinite dimensions along the coordinate axes $0x$ and $0y$ (Figure 2), with a characteristic linear dimension along the $0z$ axis – thickness L , m. The initial temperature of the soil layer (at time $t = 0$) along the coordinate interval $z \in [0; L]$ is known and is T_0 , °C. Under the influence of a radiant flux with constant intensity q , W/m^2 , the soil temperature varies along the $0z$ coordinate over time t , s. The temperature field is influenced not only by thermal conductivity but also by the transfer of thermal energy with water vapor as it moves through the soil capillaries, induced by concentration differences of the mixture components (Dufour effect). Determine the temperature distribution $T(z, t)$.

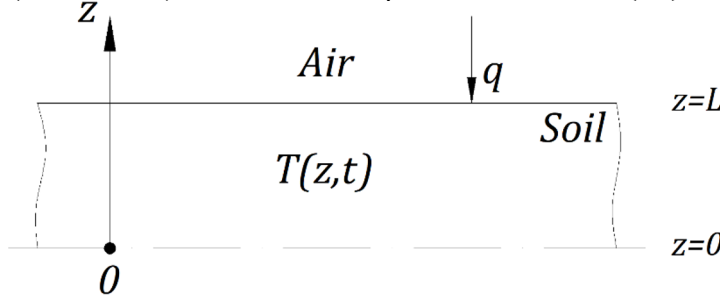


Fig. 2. Formulation of the heat transfer problem.

The portion of the thermal flux from the infrared radiation source affecting the temperature field of the soil layer is calculated using the heat balance equation for its surface:

$$q = \left(1 - \frac{R}{100} \right) q_{inf} - q_{vp} - q_{conv}, \text{ W/m}^2, \quad (7)$$

where R is the surface thermal reflectance of the soil, %; q_{inf} is the thermal flux density from the infrared radiation source, W/m^2 ; q_{vp} is the thermal flux density consumed for moisture evaporation from the soil surface (directly proportional to the evaporation intensity j), W/m^2 ; q_{conv} is the thermal flux density due to convective heat exchange between the soil surface and the surrounding environment (air), W/m^2 , determined using Newton's law of cooling.

The differential heat transfer equation, accounting for changes in the temperature field of the soil layer due to both external thermal influences and internal vapor diffusion processes (Dufour effect), along with the boundary conditions for its solution, is as follows (Figure 2):

$$\frac{\partial T(z, t)}{\partial t} = \alpha \frac{\partial^2 T(z, t)}{\partial z^2} + \frac{\varepsilon h_{fg}}{c} \frac{\partial W(z, t)}{\partial t} \quad (0 \leq z \leq L, t > 0), \quad (8)$$

$$T(z, 0) = T_0, \quad (9)$$

$$k \frac{\partial T(L, t)}{\partial z} + q = 0, \quad (10)$$

$$T(0, t) = T_0, \quad \frac{\partial T(0, t)}{\partial z} = 0, \quad (11)$$

where T is the temperature, °C; z is the coordinate, m; t is time, s; α is the soil thermal diffusivity, m^2/s ; ε is the phase transition criterion, which represents the fraction of moisture flux in the form of water vapor within the total moisture flux; h_{fg} is the latent heat of vaporization, J/kg ; c is the specific heat capacity of the soil, $\text{J}/(\text{kg} \cdot \text{K})$; k is the thermal conductivity of the soil, $\text{W}/(\text{m} \cdot \text{K})$; q is the thermal flux density at the soil surface, W/m^2 .

The solution to the heat transfer differential equation (8) with initial (9) and boundary (10), (11) conditions is known and is given by:

$$\begin{aligned}
 T(z, t) = & T_0 + \frac{qL}{k} \left[\text{Fo}_T - \frac{1}{6} \left(1 - 3 \frac{z^2}{L^2} \right) + \right. \\
 & + \sum_{n=1}^{\infty} (-1)^{n+1} \frac{2}{n^2 \pi^2} \cos \left(n \pi \frac{z}{L} \right) e^{-n^2 \pi^2 \text{Fo}_T} + \\
 & + \left. \frac{2T_0 k}{qL^2} \sum_{n=1}^{\infty} \cos \left(n \pi \frac{z}{L} \right) e^{-n^2 \pi^2 \text{Fo}_T} \cdot \int_0^L \cos \left(n \pi \frac{z}{L} \right) dz \right] + \\
 & + \frac{\varepsilon h_{fg}}{c} \frac{1}{1 - \text{Le}} \frac{jL}{D \rho} \left\{ \text{Fo}_T - \text{Fo}_W + \sum_{n=1}^{\infty} (-1)^{n+1} \frac{2}{n^2 \pi^2} \cos \left(n \pi \frac{z}{L} \right) \times \right. \\
 & \times \left[e^{-n^2 \pi^2 \text{Fo}_T} - e^{-n^2 \pi^2 \text{Fo}_W} \right] - \frac{2W_0 D \rho}{jL^2} \sum_{n=1}^{\infty} \cos \left(n \pi \frac{z}{L} \right) \times \\
 & \times \left. \left[e^{-n^2 \pi^2 \text{Fo}_T} - e^{-n^2 \pi^2 \text{Fo}_W} \right] \cdot \int_0^L \cos \left(n \pi \frac{z}{L} \right) dz \right\},
 \end{aligned} \tag{12}$$

where $\text{Fo}_T = \frac{\alpha t}{L^2}$ is the Fourier number; $\text{Le} = \frac{\alpha}{D}$ is the Lewis number.

3 Results and Discussion

Let's present the solution of the mass transfer differential equation (2) using the example of milled peat (Figure 3) with the following initial data: $L = 0.02 \text{ m}$; $\rho = 74 \text{ kg}/\text{m}^3$; $D = 2.0 \cdot 10^{-8} \text{ m}^2/\text{s}$; $W_0 = 3.7 \text{ kg}/\text{kg}$; $j = 170 \cdot 10^{-6} \text{ kg}/(\text{m}^2 \cdot \text{s})$.

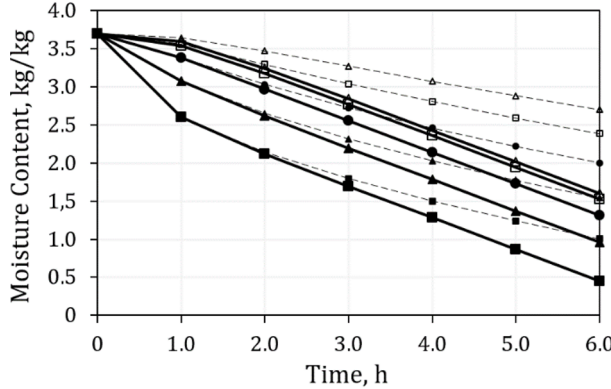


Fig. 3. Solution of the mass transfer differential equation (solid line - method of finite integral Fourier transform; dashed line - method using the error function) at z : ■ – 20 mm; ▲ – 15 mm; ● – 10 mm; □ – 5 mm; △ – 0 mm.

Over the drying period of milled peat, which is 6 hours, the average deviation in soil moisture content values (Figure 3), determined using the method of finite integral Fourier transform and the error function, does not exceed 20 %.

Let's present the solution of the heat transfer differential equation (8) using the example of milled peat (Figure 4) with the following initial data: $L = 0.02$ m; $k = 0.302$ W/(m · K); $\alpha = 14.8 \cdot 10^{-8}$ m²/s; $\rho = 74$ kg/m³; $D = 2.0 \cdot 10^{-8}$ m²/s; $Le = 7.4$; $\varepsilon = 0.1$; $h_{fg} = 2.472 \cdot 10^6$ J/kg; $c = 2.75 \cdot 10^4$ J/(kg · K); $T_0 = 5$ °C; $W_0 = 3.7$ kg/kg; $q = 100$ W/m²; $j = 170 \cdot 10^{-6}$ kg/(m² · s).

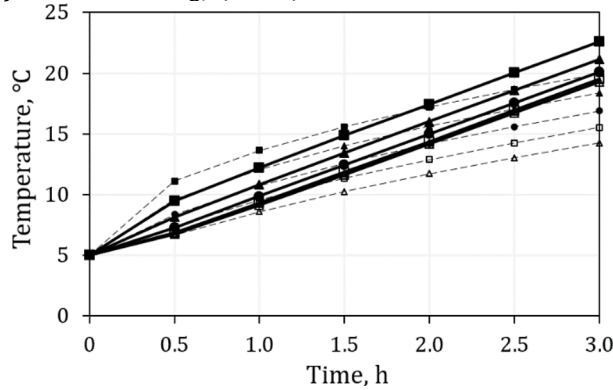


Fig. 4. Solution of the heat transfer differential equation (solid line - method of finite integral Fourier transform; dashed line - method using the error function, excluding the Dufour effect) at z : ■ – 20 mm; ▲ – 15 mm; ● – 10 mm; □ – 5 mm; △ – 0 mm.

Over the heating period of milled peat, equal to 3 hours, the average deviation of soil temperature values (Figure 4), found using the method of finite integral Fourier transform and the error function (excluding the Dufour effect), does not exceed 10 %.

Based on the mathematical solutions (6) and (12) of the heat and mass transfer differential equations (2) and (8), respectively, a program was developed in the mathematical editor Mathcad to determine the moisture content and temperature of an infinite slab.

4 Conclusions

According to the results of computational modeling, the top layer of milled peat with a thickness of 5 mm and an initial moisture content of 3.7 kg/kg will reach a final moisture content of 1.0 kg/kg in approximately 6 hours during infrared drying (Figure 3). As a result of radiant heating, the soil will reach a final temperature of 22.6 °C from an initial temperature of 5 °C in approximately 3 hours (Figure 4).

The analytical solutions of the heat and mass transfer differential equations (2) and (8), represented as algebraic functions (6) and (12), respectively, allow for the investigation of the influence of initial parameters (e.g., the intensity of moisture evaporation from the soil surface or the magnitude of heat flux density) on the soil temperature and moisture regime. This is a crucial factor in creating a favorable microclimate in cultivation structures for growing seedlings or for the growth of greens, vegetables, and flowers in protected environments. Additionally, equation (6) can be used for theoretical studies of drying capillary-porous materials (e.g., lump, ground, or milled peat), while equation (12) can be employed to manage the operation of the infrared radiation source.

At this stage of scientific research, the mass transfer differential equation (2) does not include a term accounting for the cross-process of heat and mass transfer – thermodiffusion (Soret effect) [22, 24, 25], i.e., moisture conductivity induced by the temperature gradient of the substance in the mixture. Therefore, obtaining a solution to the mass transfer differential equation using the combined application of the Laplace integral transform method [26, 34, 35] and the Bubnov-Galerkin variational method [36–38] presents

scientific interest. This approach takes into account both vapor diffusion processes (Dufour effect) and the phenomenon of thermo-moisture conductivity (Soret effect) [27–30].

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