

Thermal performance of a gas turbine based on an exergy analysis

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Abstract. This work concerns the calculation and the analysis of the thermal performance of the components of an MS 7001 type gas turbine with a nominal power of 87 MW using the concept of exergy. The exergy balance is used in addition to the energy balance to estimate the irreversibility of the air compressor, the combustion chamber and the turbine. The exergy analysis is carried out by applying the equilibrium equations obtained from the general definitions of the irreversibility of the thermodynamic processes and the data provided by the manufacturer. The results show that the exergy destruction of the gas turbine depends on the variation of the thermodynamic parameters: ambient temperature, compression ratio, air-fuel ratio. The combustion chamber has the highest exergy destruction estimated at 36.34 MW. The air compressor has an exergy efficiency of 84.19% that of the combustion chamber is 75.91% while that of the turbine expansion is 92.58%. The total exergy destruction of the gas turbine is 53.51 MW and its efficiency is 32.44%. Improving the performance of the gas turbine requires decreasing the temperature of the intake air.

1 Introduction

The present work relates to the determination of performance of a gas turbine-type GE Frame 7, rated power 87 MW, using a fuel oil of LHV 46.64 MJ / kg, the centerpiece of the mixed refrigeration loop (MR) in the Natural Gas Liquefaction process at Skikda, Algeria. The loop includes two 2 stages compressors providing a low temperature refrigeration to liquefy the natural gas in a main heat exchanger (Fig. 1). These two axial and centrifugal compressors, with a nominal capacity of 1.347419 kg / h, are driven by the gas turbine subject of this study and a start-up engine of 17 MW, mounted on the same shaft. The Mixed refrigerant (MR) used in the compressors to liquefy natural gas is a mixture of molar composition: 48.90% methane, 37.15% ethane, 8.73% propane and 5.22% nitrogen.

Since the specific atmospheric conditions in Skikda differ from ISO requirements (1 atm, 15 ° C and 60% humidity); the gas turbine performance could be affected. Its power will decrease due to high temperatures causing a decrease in the mass flow of air decreases. Efficiency also decreases because compressors require more power at a higher temperature.

The energy balance is not useful for analyzing the performance of equipment in the refrigeration loop because the real inefficiencies of the process are not related to heat loss but to exergetic destruction. Hence the use of an exergetic analysis to detect irreversibilities within the equipment of the MR loop. The evaluation of

the exergy destruction of each component in the process, will allow the assessment of the overall effectiveness of this natural gas liquefaction process. In this paper, we will limit our investigation to the examination of the gas turbine as a first objective.

Many researchers have investigated the effects of operating conditions on the performance of power plants. Al Doori [1] reportedly carried out an exergy analysis for a thermal power station in India with a 159 MW gas turbine using fuel oil (LHV = 42.9 MJ / kg). The rate of exergetic destruction in the turbine was about 5.4%, while that in the combustion chamber was about 36.4%.

Abam et al [2] performed an exergy analysis of a 33 MW gas turbine power plant in Nigeria using natural gas. The simulation results showed that the exergetic efficiency of the entire system when the temperature of air at the compressor inlet was 302 K and that of the turbine to 1087 K was 25.8 %. In addition, the combustion chamber had the highest exergetic destruction (65 MW) and the gas turbine, the lowest exergetic destruction (0.45 MW).

Kakaras [3] reported that the efficiency of the gas turbine is strongly related to the ambient air temperature. According to the gas turbine type, the output power is reduced by 5 to 10% of the rated power at 288 K according to the ISO standard for each increase of 10 K in the temperature of the ambient air. At the same time, the specific consumption of fuel increases from 1.5 to 4%.

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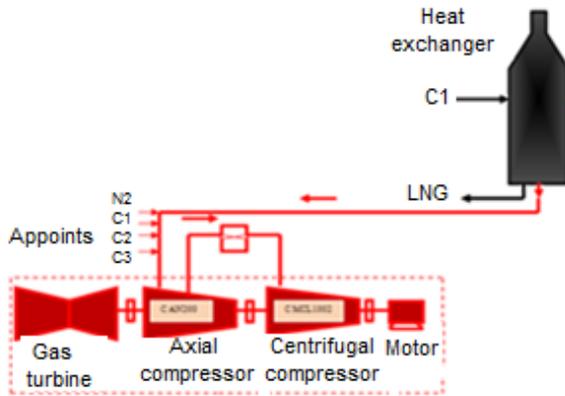


Fig. 1. Mixed refrigeration process (MR) scheme of LNG Skikda, Algeria

2 Theoretical background

Exergy is the maximum amount of useful work that can be extracted in theory from a system when it is brought to equilibrium with its environment. It is expressed by equation (1) where h_0 and s_0 are enthalpy and entropy at room temperature T_0 and at atmospheric pressure P_0 . Unlike energy, exergy depends not only on the state of the system, but also on the state of the external environment [4-6].

$$ex = (h - h_0) - T_0(s - s_0) \quad (1)$$

$$h - h_0 = C_p(T - T_0) ; \text{ Ideal gas} \quad (2)$$

$$dS = dh - vdP \quad (3)$$

$$s - s_0 = C_p \ln \frac{T}{T_0} - R \ln \frac{P}{P_0} \quad (4)$$

Combining equations (2), (3) and (4) we get:

$$ex = C_p(T - T_0) - T_0 \left(C_p \ln \frac{T}{T_0} - R \ln \frac{P}{P_0} \right) \quad (5)$$

Exergy per unit time is:

$$\dot{E}x = \dot{m} ex \quad (6)$$

The exergy balance for each component of the gas turbine (Fig. 2) will make a quantitative assessment of energy degradation, i.e. the estimation of exergy losses of each element.

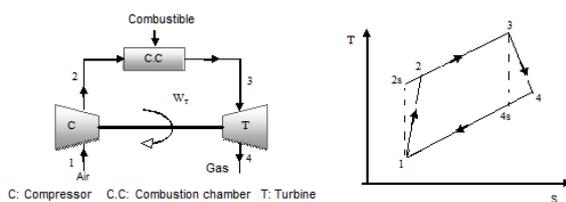


Fig. 2. Schematic diagram of the gas turbine and the associated Brayton cycle

The exergy analysis was performed by applying the above derived equations with the data provided in Table 1 and based on the schematic diagram of the components of the gas turbine (Fig. 3).

Table 1. Operating conditions used for the exergy analysis [7]

Parameters	Unit	Value
Ambient air temperature	°C	25
Air inlet pressure	Bar	1.013
Outlet compressor pressure	Bar	10.38
Inlet compressor temperature	°C	26.43
Outlet combustion chamber temperature	°C	1200
Mass flow rate of the air	kg/s	121
Mass flow rate of the fuel	Kg/s	2.69
Heat capacity of the air	J/kg.K	1005
Heat capacity of the gas	J/kg.K	1110
Specific constant of MR gas	J/kg.K	341.72
Specific constant of the air	J/kg.K	287
Adiabatic exponent		1.4
Turbine isentropic efficiency		0.87
Compressor isentropic efficiency		0.87
Compressor mechanical efficiency		0.90
Combustion chamber efficiency		0.97

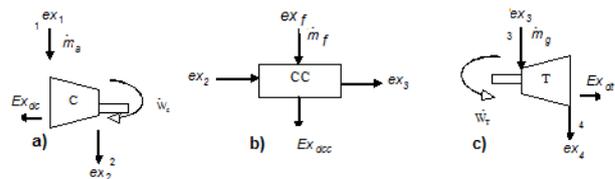


Fig. 3. Schematic diagram of the components of the gas turbine: a) C: compressor; b) CC: combustion chamber and c): T: turbine expansion

Compression section (C)

Exergy equation for the compressor:

$$\dot{m}_a ex_1 + \dot{W}_C = \dot{m}_a ex_2 + \dot{E}x_{dc} \quad (7)$$

$$Ex_{dc} = \dot{W}_C - \dot{m}_a (ex_2 - ex_1) \quad (8)$$

$$\dot{E}x_{dc} = \dot{W}_C - \dot{m}_a \left[C_{pa}(T_2 - T_1) - T_0 \left(C_{pa} \ln \frac{T_2}{T_1} - R_a \ln \frac{P_2}{P_1} \right) \right] \quad (9)$$

$$\dot{W}_C = \frac{\dot{m}_a C_{pa}(T_2 - T_1)}{\eta_m} \quad (10)$$

From the equation governing the isentropic transformation and from the definition of the isentropic

efficiency, temperatures in the compressor output will be determined:

$$\frac{T_{2s}}{T_1} = \left(\frac{P_2}{P_1}\right)^{\frac{\gamma-1}{\gamma}} = \tau^{\frac{\gamma-1}{\gamma}} \Rightarrow T_{2s} = T_1 \times \tau^{\frac{\gamma-1}{\gamma}} \quad (11)$$

$$\eta_{sc} = \frac{T_{2s}-T_1}{T_2-T_1} \Rightarrow T_2 = T_1 + \frac{T_{2s}-T_1}{\eta_{sc}} \quad (12)$$

Exergy efficiency of the compressor is given by the following equation:

$$\varepsilon_{ex\ c} = \frac{W_c - \dot{E}x_{dc}}{\dot{W}_c} = \frac{\dot{m}_a(ex_2 - ex_1)}{\dot{W}_c} \quad (13)$$

Combustion section (CC)

Exergy equation for the combustion chamber:

$$\dot{m}_a ex_2 + \dot{m}_f ex_f = \dot{m}_g ex_3 + \dot{E}x_{dcc} \quad (14)$$

$$\dot{E}x_{dcc} = \dot{m}_a ex_2 + \dot{m}_f ex_f - \dot{m}_g ex_3 \quad (15)$$

The exergy of the fuel is determined by:

$$ex_f = \gamma_f \cdot PCI \quad (16)$$

$\gamma_f = 1.02$ is the exergy factor based on the lower calorific value of the fuel used.

$$\begin{aligned} \dot{E}x_{dcc} = \dot{m}_a \left[C_{pa}(T_2 - T_0) - T_0 \left(C_{pa} \ln \frac{T_2}{T_0} - \right. \right. \\ \left. \left. R_a \ln \frac{P_2}{P_0} \right) \right] + \dot{m}_f (\gamma_f \cdot PCI) - \dot{m}_g \left[C_{pg}(T_3 - T_0) - \right. \\ \left. T_0 \left(C_{pg} \ln \frac{T_3}{T_0} - R_g \ln \frac{P_3}{P_0} \right) \right] \end{aligned} \quad (17)$$

The mass flow rate of natural gas in the combustion chamber is determined by the ratio:

$$f = \frac{Q_{cc}}{PCI} = \frac{\dot{m}_f}{\dot{m}_a} \quad (18)$$

Q_{cc} is the heat of combustion determined by:

$$Q_{cc} = \frac{C_{pg}T_3 - C_{pa}T_2}{\eta_{cc}} \quad (19)$$

Exergy efficiency of the combustion chamber :

$$\varepsilon_{ex\ cc} = \frac{\dot{m}_g ex_3}{\dot{m}_a ex_2 + \dot{m}_f ex_f} = 1 - \frac{\dot{E}x_{dcc}}{\dot{m}_a ex_2 + \dot{m}_f (\gamma_f \cdot PCI)} \quad (20)$$

Expansion section (T):

The balance equation Exergy expansion section of the turbine is given by:

$$\dot{m}_g ex_3 = \dot{W}_T + \dot{E}x_{dT} + \dot{m}_g ex_4 \quad (21)$$

$$\dot{E}x_{dT} = \dot{m}_g (ex_3 - ex_4) - \dot{W}_T \quad (22)$$

$$\begin{aligned} \dot{E}x_{dT} = \dot{m}_g \left[C_{pg}(T_3 - T_4) - T_0 \left(C_{pg} \ln \frac{T_3}{T_4} - R_g \ln \frac{P_3}{P_4} \right) \right] \\ - \dot{W}_T \end{aligned} \quad (23)$$

$$\eta_{sT} = \frac{W_T}{W_{sT}} \Rightarrow W_T = \eta_{sT} \cdot \quad (24)$$

$$\dot{W}_{sT} = \dot{m}_g C_{pg}(T_3 - T_{4s}) \quad (25)$$

$$\frac{T_3}{P_3^{\frac{\gamma-1}{\gamma}}} = \frac{T_{4s}}{P_{4s}^{\frac{\gamma-1}{\gamma}}} \Rightarrow T_{4s} = T_3 \cdot \left(\frac{P_{4s}}{P_3}\right)^{\frac{\gamma-1}{\gamma}} \quad (26)$$

$$T_{4s} = T_3 \left(\frac{P_4}{P_3}\right)^{\frac{\gamma-1}{\gamma}} = T_3 \cdot \left(\frac{P_1}{P_2}\right)^{\frac{\gamma-1}{\gamma}} = T_3 \cdot \left(\frac{1}{\tau}\right)^{\frac{\gamma-1}{\gamma}} \quad (27)$$

Turbine outlet temperature T_4 :

$$\eta_{sT} = \frac{T_3 - T_4}{T_3 - T_{4s}} \Rightarrow T_4 = T_3 - \eta_{sT}(T_3 - T_{4s}) \quad (28)$$

Exergy efficiency of the expansion through the turbine:

$$\varepsilon_{ex\ T} = \frac{\dot{W}_T}{\dot{m}_g (ex_3 - ex_4)} \quad (29)$$

$$\varepsilon_{ex\ T} = 1 - \frac{\dot{E}x_{dT}}{\dot{m}_g (ex_3 - ex_4)} \quad (30)$$

3. Results and discussion

Exergy analysis results of the gas turbine according to the given operating conditions are shown in Table 2 and Figures 4, 5 and 6.

Table 2. Exergy analysis results of the gas turbine according to the operating conditions (Tab. 1).

Component	$\dot{E}x_d$ (MW)	(%) $\dot{E}x_d$	ε_{ex} (%)
Compressor (C)	6.94	12.96	84.19
Combustion chamber (CC)	39.73	74.24	75.91
Turbine expansion (T)	6.84	12.80	92.58
Gas turbine	53.51	100	32.44

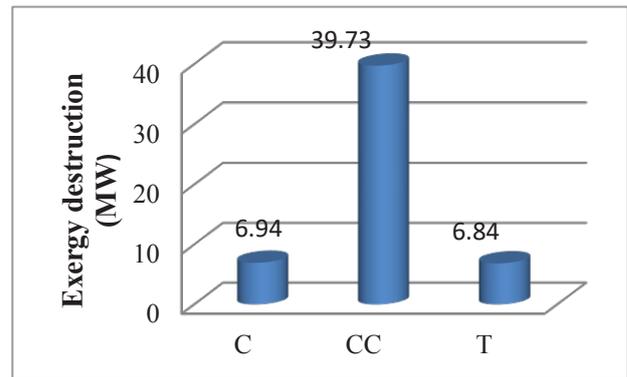


Fig. 4. Distribution of Exergy destruction at each component of the gas turbine

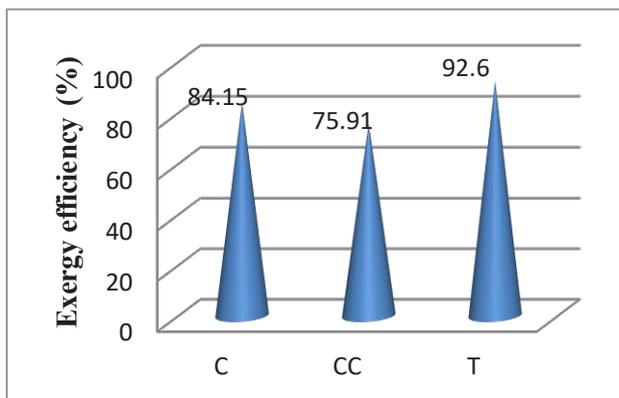


Fig. 5. Exergy efficiency of each component of the gas turbine

The maximum exergy destruction is in the combustion chamber and is 39.73 MW. For this reason, its exergy efficiency is the lowest compared to other components of the gas turbine. The values of the exergy efficiency are respectively: 84.19% for the compressor, 75.91% for the combustion chamber and 92.58% for the expansion through the turbine.

Global Exergy destruction of the gas turbine will be the sum of the destruction in the 03 components:

$$\dot{E}x_d = 53.51 \text{ MW}$$

The Exergy efficiency of the gas turbine in the operating conditions will be determined by:

$$\varepsilon_{Tgaz} = \frac{\dot{W}_U}{\dot{Q}_{cc}} = \frac{\dot{W}_T - \dot{W}_C}{\dot{Q}_{cc}} = \frac{85.44 - 43.91}{128} = 32.44 \%$$

The exergy destruction of the gas turbine depends on the variation of thermodynamic variables: pressure and temperature, for deduction of the compression ratio and the air-fuel ratio. The operating conditions of the gas turbine are decisive in the analysis of its thermodynamic performance. For this, the exergy analysis was performed according to the variation of the ambient air intake temperature to the compressor between -2 and 45 ° C. The performance results of the gas turbine as a function of the variation of the ambient air temperature are summarized in Table 3 and Figures 6 and 7.

Table 3. Evolution of exergy performance of the gas turbine as a function of the change in ambient air temperature T_1

T_1 (K)	\dot{W}_C (MW)	$\dot{E}x_{dc}$ (MW)	ε_{exc} (%)	$\dot{E}x_{dcc}$ (MW)	ε_{excc} (%)	ε_{exTgaz} (%)
271.2	39.78	6.53	83.58	32.75	79.27	35.67
276.4	40.52	6.60	83.71	34.08	78.60	35.09
281.6	41.28	6.63	83.93	35.37	77.97	34.50
286.8	42.05	6.75	83.95	36.63	77.37	33.89
292	42.80	6.82	84.06	37.97	76.73	33.31
297.3	43.59	6.91	84.15	39.31	76.11	32.69
299.4	43.91	6.94	84.19	39.73	75.91	32.44
302.5	44.34	6.97	84.28	40.66	75.49	32.11
307.7	45.11	7.05	84.37	41.96	74.90	31.50
312.9	45.87	7.13	84.45	43.30	74.30	30.91
318.2	46.65	7.21	84.54	44.62	73.73	30.30

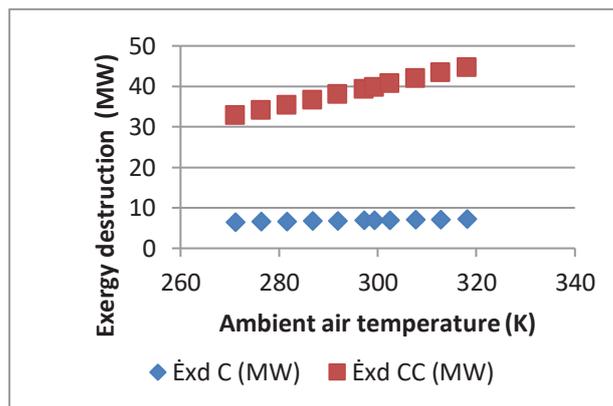


Fig. 6. Evolution of exergy destruction of the gas turbine as a function of the change in ambient air temperature T_1

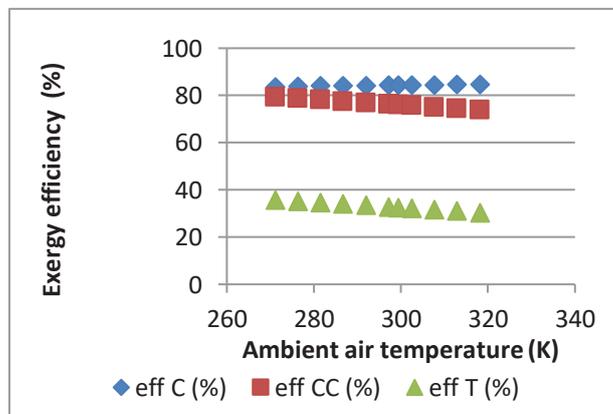


Fig. 7. Evolution of exergy efficiency of the gas turbine as a function of the change in ambient air temperature T_1

During the increase of the ambient air temperature from 271 K to 318 K (-2 to 45 ° C), the exergetic destruction increases slightly in the compressor from 6.53 to 7.21 MW, it increases more significantly within the chamber combustion from 32.75 to 44.62 MW (Fig. 6); while the exergy efficiency goes from 83.58% to 84.54% for the compressor, decreases from 79.27 to 73.73% for the combustion chamber; that of the gas turbine as a whole decreases from 35.67 to 30.30% (Fig. 7).

An increase in air temperature causes a small increase in the exergy destruction of the compressor. Increasing the temperature of ambient air will also increase the exergy destruction in the combustion chamber and decrease the exergy destruction in the turbine.

4 Conclusion

The Exergy balance of a thermodynamic system allows the determination of the Exergy destruction or the estimate of the energy losses due to the irreversibility of actual transformations. This leads to the quantitative measurement of the Exergy efficiency. The results show that the efficiency of the combustion chamber is the lowest compared to that of the compressor and the expansion in the turbine because it is where the highest exergy destruction takes place. The total exergy destruction of the 84.55MW gas turbine is 53.51 MW and its efficiency is 32.44% in the operating conditions. The change in ambient temperature has a direct impact on the exergy performance of the gas turbine. Exergy destruction increases with air increase in temperature while the exergy efficiency decreases. The effects of air humidity, of compression ratio and fuel air ratio inside the combustion chamber on the performance of the gas turbine will be examined shortly.

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