

Evaluation of a counter-flow microchannel heat exchanger performance with air-water vapor mixture to liquid water

C. Ren¹, J. H. Weng^{1,*}, J. N. Yan¹, L. Wang¹, H. L. She², and X. Y. Cui²

¹School of Energy & Mechanical Engineering, Shanghai University of Electric Power, Shanghai 200090

²School of Energy and Power Engineering, University of Shanghai for Science and Technology, Shanghai 200093

Abstract. Given its configuration and operation conditions, the performance of a counter-flow microchannel heat exchanger (MCHX) is evaluated through detailed calculations. The fluids, both liquid water and air, are considered as continuum flow flowing in microchannels. The MCHX has 59 sheets, and each sheet has 48 microchannels. The microchannels for both fluids have the same cross section of 0.8mm×1mm and same length of 200mm. Log mean temperature difference method is adopted for this evaluation. Using appropriate equations, the properties of air-water vapor mixture are calculated based on that of the two components. Given the inlet temperature for liquid water(35°C) and air (170°C), the calculated outlet temperature for both fluids are 55.5°C and 43.3°C, respectively. The results also show that the air at the outlet is saturated. The overall heat transfer coefficient reaches 100W/m²·K, which is much higher than that of conventional heat exchanger with similar fluid combinations.

1 Introduction

Microchannel heat exchangers (MCHXs) have been increasingly attractive in many applications such as energy system, electronic cooling, fuel cell automobiles, etc.. They have advantages of small size, light in weight, less materials, and high heat transfer coefficients. In addition, they have very high surface area to volume ratios. Heat exchangers are usually critical components in energy systems and more and more MCHXs are used due to their advantages. In a waste heat recovery and energy conversion system [1], a nominal 10.6KW cross-counter MCHX was designed and fabricated. Oil was used to recover the heat of the exhaust gases from a diesel engine in a MCHX. The microchannel is 2mm in width and 0.8mm in depth on the exhaust side, and 1.5mm in width and 0.15mm in depth on the oil side. The MCHX was fabricated by photochemical etching and diffusion brazing processes. In another application, D. A. Kromer et al. [2] designed, fabricated and evaluated a type of stainless steel MCHXs used in a new reactor system. The MCHXs were arranged in groups in the system for heat exchanging between the primary and secondary coolant. The cross-section of the channels for both coolant is close to a semi-circular, with a flat bottom. The height and width of the channel are 0.635mm and 1.397mm, respectively. The photochemical etching and diffusion bonding processes were used to fabricate the MCHXs. For high temperature gas-gas heat exchanging, a ceramic counter-counter flow MCHX was designed, fabricated and evaluated [3]. Ceramic materials allow the MCHX to be operated at very high temperature or in a harsh chemical

environment. The MCHX was tested with hot air inlet temperature up to 750°C. The microchannel is approximately 550µm in height and 2.8mm in width.

MCHXs are also attractive to high-heat-flux thermal management. A copper alloy microchannel heat exchanger with overall dimensions of 1cm×1cm×1cm was designed and fabricated using micro-electro-discharge machining(µEDM) [4]. The MCHX was used to remove the heat from a closed-loop flow of refrigerant R245fa by air. The flow passage for air is circular and has a diameter of 520µm, while that for refrigerant R245fa is rectangular and has a size of 0.5mm×2mm. The rate of heat transfer for the cross-flow MCHX reaches up to 60W.

In this paper, a MCHX with air-water vapor mixture as hot fluid and liquid water as cold fluid is evaluated by detailed calculations. The air-water vapor mixture is cooled by liquid water. Given inlet temperature for both fluids, the heat load is calculated through an iteration process. It is found water vapor in the air starts to condense at somewhere along the flow passage and the air at the outlet is saturated. Improvements for the MCHX design are also discussed.

2 MCHX configuration

The MCHX consists of 59 sheets, alternating between air and liquid water sheets (Fig. 1). Each sheet has 48 microchannels. The cross-section of the microchannel for both fluids has a same size of 0.8mm×1mm. The length of the microchannel for both fluids also is same, which is 200mm (Fig. 2). The two fluids flow in the opposite direction, which makes the MCHX a counter

* Corresponding author: jhweng@shiep.edu.cn

flow heat exchanger. The materials of the MCHX is stainless steel, and the microchannel is micro-fabricated on each sheet.

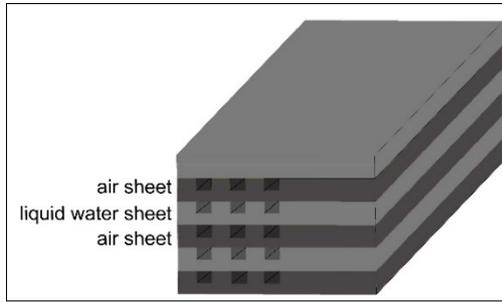


Fig. 1. Sheet arrangement for MCHX.

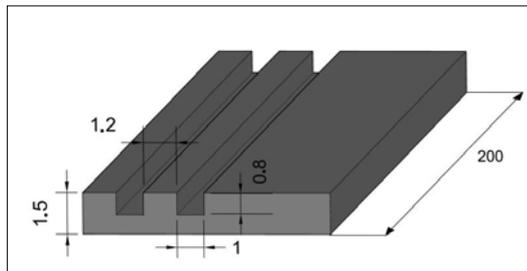


Fig. 2. Sheet arrangement for MCHX.

Table 1. MCHX channel dimensions.

Parameter	Value
Channel height/mm	0.8
Channel width/mm	1.0
Channel length/mm	200
Hydraulic diameter/mm	0.8889

3 Performance evaluation method

3.1 Flow regime

The flow in microchannel can be classified into 4 regimes according to the Knudsen number Kn . For Kn less than 0.001, the flow is a continuum flow and can be accurately modeled by N-S equations with classical no-slip boundary conditions. And correlations developed for conventional macrochannels are mostly valid for microchannel predictions, although sometimes divergences were found. In this study, the pressure of air flow is around 1atm, and the inlet temperature is 170°C. Using the below equation [5]:

$$Kn = \frac{\lambda}{L} \quad (1)$$

where $k_2 = 1.277$, and

$$\lambda = k_2 \frac{\mu}{\rho \sqrt{RT}} \quad (2)$$

the calculated Kn number is 0.000123 in this study, which is less than 0.001 for the air flowing in microchannels. Correlations for macrochannel flow are used for the calculation of air stream below.

3.2 Thermal properties of air-water vapor mixture

The air stream is cooled while heating the water in the MCHX. The air stream consists of dry air and water vapor, and it is a mixture of the two components. The dynamic viscosity and thermal conductivity are calculated with the following equations [6]:

$$\mu_a = \frac{x_{da}\mu_{da}}{x_{da} + x_v\phi_{12}} + \frac{x_v\mu_v}{x_v + x_{da}\phi_{21}} \quad (3)$$

$$\lambda_a = \frac{x_{da}\lambda_{da}}{x_{da} + x_v\phi_{12}} + \frac{x_v\lambda_v}{x_v + x_{da}\phi_{21}} \quad (4)$$

where,

$$\phi_{ij} = \frac{[1 + (\mu_i / \mu_j)^{1/2} (M_j / M_i)^{1/4}]^2}{[8(1 + M_i / M_j)]^{1/2}} \quad (5)$$

3.3 Overall heat transfer coefficient

As the thermal conductivity of the stainless steel is relatively high, the thermal resistance of the solid wall of the MCHX is neglected for simplicity in this study. Also as the areas of the channels for both fluids are equal, the overall heat transfer coefficient can be written as:

$$\frac{1}{U} = \frac{1}{h_{ca}} + \frac{1}{h_{cw}} \quad (6)$$

For fully developed laminar flow in rectangular channel(constant wall temperature) [5],

$$Nu = 7.541(1 - 2.610\alpha + 4.970\alpha^2 - 5.119\alpha^3 + 2.702\alpha^4 - 0.548\alpha^5) \quad (7)$$

where α is the channel aspect ratio a/b . And convection heat transfer coefficients for both fluids are calculated using the above equation.

3.4 Heat transfer calculation

Given the inlet temperature of air and liquid water and the MCHX configuration, a heat transfer rate Q' is first assumed for the calculation. Then the outlet temperature of the liquid water and air-water vapor mixture are determined from below equations [7-8]:

$$Q_w = q_{mw}C_{pw}(t_{wo} - t_{wi}) \quad (8)$$

$$Q_a = q_{ma}(h_{ao} - h_{ai}) - q_{mcw}h_w \quad (9)$$

Equation (9) is used as the air is already saturated at the outlet, and water-vapor condensation happens during

the cooling of the air. The enthalpy of air per unit mass of dry air is

$$h = h_a + dh_v \quad (10)$$

After the determination of outlet temperature, the log mean temperature difference is calculated (for counter flow heat exchanger):

$$\Delta t_m = \frac{\Delta t_{\max} - \Delta t_{\min}}{\ln \frac{\Delta t_{\max}}{\Delta t_{\min}}} \quad (11)$$

The heat transfer rate between liquid water and air-water vapor is calculated:

$$Q = UA\Delta t_m \quad (12)$$

The calculated heat transfer rate Q is then compared with the assumed Q' . If the two are close (e.g. less than 5%), the iteration process is terminated. Otherwise a new Q' is assumed and the iteration process continues.

3.5 Pressure drop calculation

For fully developed laminar flow in microchannels, as both fluids are considered as continuum flow, the Fanning friction factor can be calculated from the below equation [5]:

$$f Re = 24(1 - 1.3553\alpha + 1.9467\alpha^2 - 1.7012\alpha^3 + 0.9564\alpha^4 - 0.2574\alpha^5) \quad (13)$$

The pressure drop for both fluids are

$$\Delta p = \frac{2f\rho u^2 L}{D_h} \quad (14)$$

4 Results and discussions

For the MCHX in this study, the inlet temperature of air is 170°C, with a humidity ratio 150g water vapor per kg dry air. The inlet temperature of liquid water is 35°C. The two fluids flow in a counter-flow condition. Using the above method, the outlet temperature for both liquid water and air, as well as the heat load of the MCHX are obtained through the iteration process. The evaluation results are shown in Table 2. The outlet temperature for liquid water and air are 55.5°C and 43.3°C, respectively. And the heat load of the MCHX is about 4.1kW. The air at the outlet is saturated and certain amount of water vapor is condensed. The pressure drop for liquid water and air are 0.202kPa and 1.884kPa, respectively. Fluid properties are summarized in Table 3. The design of the MCHX has much room for optimization. For example, the convection heat transfer coefficient of the air side is much lower than that of the liquid water side, and increasing the convective heat transfer coefficient of the air side could efficiently increase the overall heat transfer coefficient, which can improve the MCHX overall performance. This could be done by turning the air into turbulent flow, etc..

Table 2. Evaluation results summary.

	Value
Air side	
Velocity/m·s ⁻¹	12.49
Re	484
Nu	3.01
Convection heat transfer coefficient/W·m ⁻² ·K ⁻¹	105.0
Outlet temperature/°C	43.3
Heat transfer rate from air side/kW	4.205
Pressure drop/kPa	1.884
Liquid water side	
Velocity/m·s ⁻¹	0.045
Re	65
Nu	3.01
Convection heat transfer coefficient/W·m ⁻² ·K ⁻¹	2146.5
Outlet temperature/°C	55.5
Heat transfer rate from water side/kW	4.205
Pressure drop/kPa	0.202
Overall heat transfer coefficient/W·m ⁻² ·K ⁻¹	100.1
Mean temperature difference/°C	40.5
Heat transfer rate/kW	4.054

Table 3. Fluid properties summary.

	Value
Air side (mixture of dry air and water vapor)	
Density at inlet/kg·m ⁻³	0.7377
Density at outlet/kg·m ⁻³	1.0466
Thermal conductivity at inlet/W·m ⁻¹ ·K ⁻¹	0.0357
Thermal conductivity at outlet/W·m ⁻¹ ·K ⁻¹	0.0264
Dynamic viscosity at inlet/kg·m ⁻¹ ·s ⁻¹	2.2906×10 ⁻⁵
Dynamic viscosity at inlet/kg·m ⁻¹ ·s ⁻¹	1.8540×10 ⁻⁵
Liquid water side	
Density at inlet/kg·m ⁻³	994.0
Density at outlet/kg·m ⁻³	985.2
Thermal conductivity at inlet/W·m ⁻¹ ·K ⁻¹	0.623
Thermal conductivity at outlet/W·m ⁻¹ ·K ⁻¹	0.649
Dynamic viscosity at inlet/kg·m ⁻¹ ·s ⁻¹	7.20×10 ⁻⁴
Dynamic viscosity at inlet/kg·m ⁻¹ ·s ⁻¹	5.04×10 ⁻⁴

5 Conclusions

The performance of a counter-flow MCHX is evaluated and the heat load and pressure drops of both water and air side are obtained. The air is cooled while the liquid water is heated. Based on the Kn number, the air flow can be considered as continuum flow, so correlations for macrochannel flow are used for the calculation. Thermal properties of the air stream, which is a mixture of dry air and water vapor, are calculated with the properties of the two components. The air at the outlet is saturated and

certain amount of water vapor is condensed. Comparing with the convection heat transfer coefficient of water side, the convection heat transfer coefficient of air side is relative low. Configurations of the MCHX should be optimized to improve the heat exchanger performance. When water is replaced by methanol-water solution, the MCHX can be used as a heat exchanger in the power system of fuel cell automobile. MCHX, as highly compact heat exchanger, can be used in various applications, such as energy system, automobile, etc.. The MCHXs are expected to have wide applications in industry due to their advantages.

Nomenclature

<i>Variables</i>	α : aspect ratio, a/b
A: area, m ²	ρ : density, kg/m ³
a: channel height, m	λ : thermal conductivity, W/m ² ·K; mean free path, m
b: channel width, m	μ : dynamic viscosity, kg/m·s
C _p : specific heat, J/kg·K	
D _h : hydraulic diameter, m	
d: specific humidity, kg/kg	
f: Fanning friction factor	<i>Subscripts</i>
h: specific enthalpy, J/kg;	a: air side
h _c : convection heat transfer coefficient, W/m ² ·K	da: dry air
Kn: Knudsen number	i: inlet
L: channel length, m	i, j: component
M: molar mass, kg/kmol	o: outlet
Nu: Nusselt number	v: water vapor
Δp : pressure drop, Pa	w: water side
Q: heat transfer rate, W	o: outlet
q _m : mass flow rate, kg/s	
R: Gas constant, J/kg·K	
Re: Reynolds number	
T: temperature, K	
t: temperature, °C	
Δt : temperature difference, °C	
U: overall heat transfer coefficient, W/m ² ·K	
u: velocity, m/s	
x: mole fraction	

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