

Experimental study on the influencing factors of SBBR nitrosation controlled by sodium chlorate inhibitor

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Abstract. The research takes low C/N ratio sewage as the research object, and quickly realizes the accumulation of nitrite nitrogen by adding inhibitors into the SBBR reactor, and realizes the nitrogen removal by anaerobic ammonia oxidation in the reactor. Determining the optimal operating parameters is of far-reaching significance for the treatment of wastewater with high ammonia nitrogen and low C/N and achieving economical and efficient nitrogen removal. Control the ammonia oxidation reaction, keep the nitrification process in the nitrosation stage, and realize the rapid accumulation of NO₂-N is the problem that the reactor needs to solve. This experiment uses a combination of batch test and periodic test to conduct experimental research on various influencing factors in the partial nitrosation process: temperature, pH, DO and find the best operating conditions to achieve high-efficiency accumulation of NO₂-N and optimize the reaction conditions.

1 Introduction

SBBR (Sequencing batch biofilm reactor) is a biological denitrification process developed on the basis of the SBR process. The activated sludge method and the biofilm method are organically combined with different fillers in the reactor as the growth environment for microorganisms. A method of combining [1]. The filler has a certain effect on the treatment effect of the SBBR reactor, and PU sponge is used as a filler [2]. This research takes SBBR process as the main body and polyurethane sponge as the filler. The experiment is equipped with R1 and R2 reactors. R1 uses sodium chlorate inhibitor for culture and R2 uses traditional culture methods to domesticate the sludge which is contrasted with R1. Through experimental research on various influencing factors in the nitrosation process: temperature, pH and DO, the optimal reaction conditions are found to provide theoretical support for optimizing the reaction device. The experimental setup is shown in Figure 1.

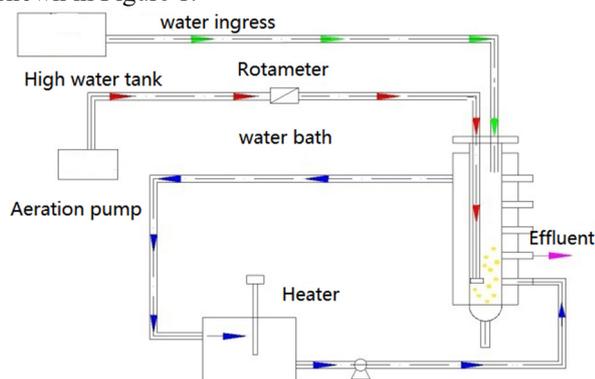


Fig1.. Schematic diagram of SBBR reaction device

2 The influence of temperature on nitrosation reaction

The environmental factors at this stage are controlled as follows: control the R1 inlet water NH₄⁺-N to 150mg·L⁻¹, add NaClO₃ to a concentration of 1.0mol·L⁻¹, pH stabilized between 7.5 and 8.0, adjust the gas flowmeter to control the aeration volume It is 300~400mL·min⁻¹ to stabilize the DO concentration at about 0.5mg·L⁻¹. Set the temperature gradient to 15°C, 20°C, 25°C, 28°C, 30°C, 32°C and 35°C. The reactor adopts the operation mode of water intake (instantaneous)-aeration (4h)-sedimentation (2h)-drainage (instantaneous)-idle (2h). It runs 3 cycles per day and runs continuously for 7 days. Regularly check the various indicators of the incoming and outgoing water every day to investigate the effect of temperature on the removal of NH₄⁺-N and the effect of NO₂⁻-N accumulation. The test results are shown in Figure 2 and Figure 3.

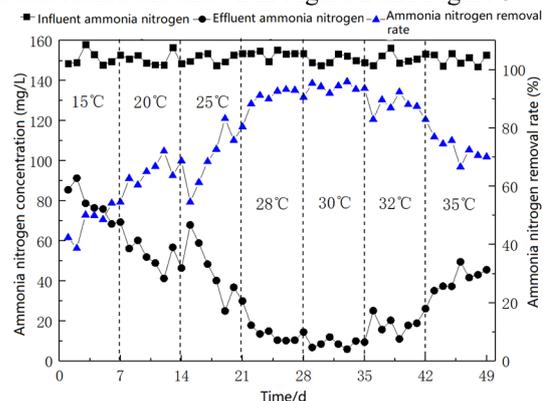


Fig2. The effect of temperature on the removal effect of NH₄⁺-N

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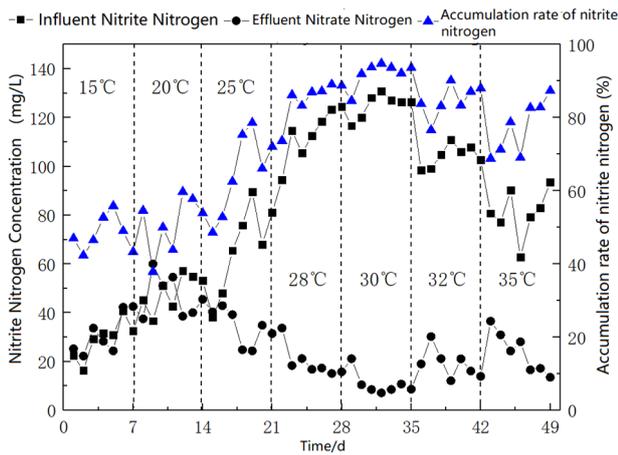


Fig3. The influence of temperature on NO_2^- -N accumulation effect

It can be seen from Figure 2 that when the control temperature is between 28°C and 32°C , the NH_4^+ -N removal rate in the reactor is very high, and the average removal rate of NH_4^+ -N is 90.86%; The effluent NH_4^+ -N concentration is also relatively stable, and the average effluent NH_4^+ -N concentration is $13.76\text{mg}\cdot\text{L}^{-1}$. Both the highest NH_4^+ -N removal rate and the lowest effluent NH_4^+ -N concentration are within this range (both at 30°C), and the nitrifying bacteria are extremely active and have the best metabolism. When the temperature is low (20°C) or high (35°C), the NH_4^+ -N removal effect is average, and the curve drops when the temperature is high. When the temperature is 25°C , the removal rate of NH_4^+ -N is low, only 54.61%. After timely repair, the removal rate of NH_4^+ -N is significantly improved, and the water output effect is optimized again.

Analyzing Figure 3 found that when the reactor is at 15°C and 20°C , the accumulation effect of NO_2^- -N is general. With the further increase of the temperature in the reactor, the NO_2^- -N concentration in the effluent rose significantly during the 7d test time at 25°C , from the initial $38.2\text{mg}\cdot\text{L}^{-1}$ to $89.6\text{mg}\cdot\text{L}^{-1}$, the average accumulation rate of NO_2^- -N reaches 66.65%; at 28°C , the effluent quality is optimized, the NO_3^- -N concentration of effluent is lower than $20\text{mg}\cdot\text{L}^{-1}$, NO_2^- -N accumulation is stable, and the fluctuation is small; the reaction is further optimized at 30°C . At this stage, the reactor has the highest NO_2^- -N accumulation rate, which is 94.81%; the average concentration of NO_3^- -N in the effluent is only $10.76\text{mg}\cdot\text{L}^{-1}$. At 32°C and 35°C , although the accumulation of NO_2^- -N is still considerable, the concentration of NO_2^- -N and NO_3^- -N in the effluent changes greatly, and the water quality is relatively poor, which is not conducive to the stable operation of the nitrification reaction.

The test results show that temperature is an important factor affecting the nitrification reaction. When the microorganisms are at different temperatures, the removal rate of NH_4^+ -N and the accumulation rate of NO_2^- -N have obvious differences. When the temperature is controlled at about $28\sim 30^\circ\text{C}$, the effluent quality is in line with expectations. When the temperature is low, the effluent quality is poor, the effluent NO_2^- -N and NO_3^- -N concentrations are similar, and the effluent NH_4^+ -N

concentration is higher. When the temperature is high, the removal rate of NH_4^+ -N and the accumulation rate of NO_2^- -N both decrease to varying degrees. In summary, the optimum temperature range for the nitrification process is $28\sim 30^\circ\text{C}$, and the best temperature is around 30°C . This is similar to the results of Yoo [3].

3 The influence of pH on nitrification reaction

The specific operation method of the test is as follows: control the temperature at $(28\pm 1)^\circ\text{C}$, maintain the DO concentration between 0.5 and 1.0 mg/L, the influent NH_4^+ -N concentration at about $150\text{mg}\cdot\text{L}^{-1}$, run 2 cycles per day, single The cycle process is water intake (instantaneous)-aeration (6h)-sedimentation (3h)-drainage (instantaneous)-idle (3h). The test uses 10% dilute hydrochloric acid and sodium bicarbonate solution to adjust the pH value, and conducts 3 batches of tests. Each batch is for 2 sets of parallel tests, and the pH is controlled between 6.0, 6.5, 7.0, 7.5, 8.0, and 8.5. Each batch was run for 7 days, and various water inlet and outlet indicators were checked regularly to investigate the influence of pH on the removal effect of NH_4^+ -N and the effect of NO_2^- -N accumulation. The test results are shown in Figure 4 and Figure 5.

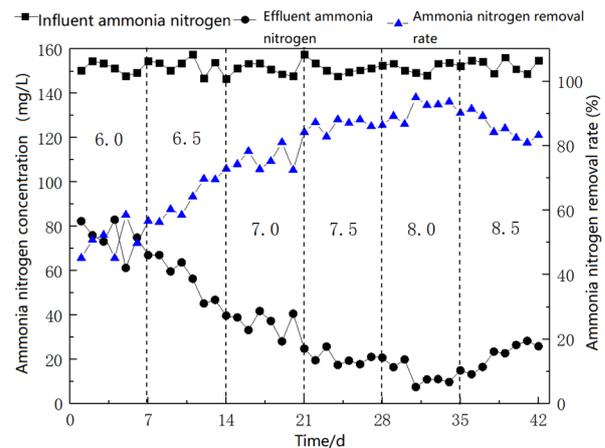


Fig4. The effect of pH on the removal of NH_4^+ -N

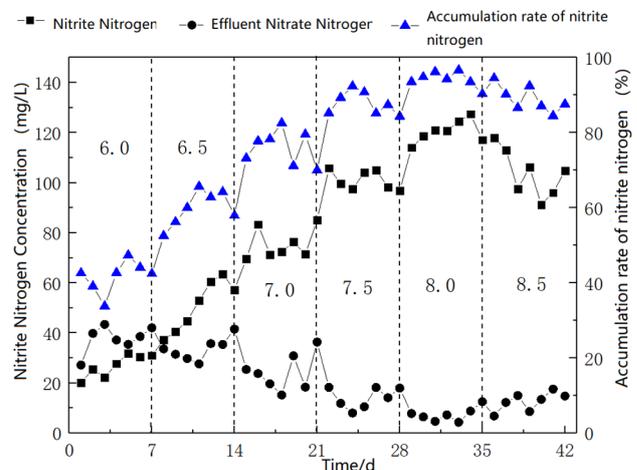


Fig5. The effect of pH on the accumulation of NO_2^- -N

It can be seen from Figure 4 that when the microorganisms are in an alkaline environment, the $\text{NH}_4^+\text{-N}$ removal effect is better, with an average removal rate of 87.86%, which is 20% higher than that of acidic conditions. When the pH is 6.0, the average concentration of $\text{NH}_4^+\text{-N}$ in the effluent is $73.95\text{mg}\cdot\text{L}^{-1}$. Observing the No. 2 reactor, when the pH is 6.5, the removal effect of $\text{NH}_4^+\text{-N}$ is average. Analyzing the data of the second set of parallel experiments (pH=7.0, pH=7.5), it was found that the microbial activity was higher at this stage, the effluent quality was better, and the removal of $\text{NH}_4^+\text{-N}$ was stable at pH 7.5, and the average removal rate was high. When the pH value is 8.0, the average removal rate of $\text{NH}_4^+\text{-N}$ at this stage is the highest, 91.44%, indicating that the microbial activity is the best at this stage, and the removal rate of No. 2 reactor during the same period is also considerable.

As shown in Figure 5, as the pH increases, the $\text{NO}_2^-\text{-N}$ concentration in the effluent rises simultaneously, and the $\text{NO}_2^-\text{-N}$ accumulation effect becomes better and better. Under acidic conditions, the effluent $\text{NO}_2^-\text{-N}$ concentration is not much different from the effluent $\text{NO}_3^-\text{-N}$ concentration, and the reactor system behaves as traditional nitric acid nitrification [4]. When the pH value increases to 7.0 and 7.5, the effluent water quality is optimized, and the average concentration of $\text{NO}_2^-\text{-N}$ in the effluent is $75.69\text{mg}\cdot\text{L}^{-1}$ and $101.04\text{mg}\cdot\text{L}^{-1}$. The system has a higher accumulation rate of $\text{NO}_2^-\text{-N}$; When the pH in the reactor reaches 8.5, the accumulation rate of $\text{NO}_2^-\text{-N}$ remains at a high level, with an average accumulation rate of 88.01%.

The test results show that the pH value has an important influence on the nitrosation reaction, and controlling the pH between 7.5 and 8.0 in an alkaline environment is conducive to the realization of the nitrosation reaction [5].

4 The influence of DO on nitrosation reaction

Nitrifying bacteria belong to the aerobic flora. Studies have found that the oxygen half-saturation constant of NOB is greater than that of AOB. The concentration of DO is vital to promote the renewal of biofilms and the formation of sludge granulation Role [6].

The specific operation method of the test is as follows: control the R1 inlet water $\text{NH}_4^+\text{-N}$ concentration to about $150\text{mg}\cdot\text{L}^{-1}$, pH between 7.5 and 8.0, and the specified temperature range at about 28°C . The operating state of the SBBR reactor is: water inlet (instantaneous)-Aeration (6h)-Sedimentation (3h)-Drainage (instantaneous)-Idle (3h), run 2 complete cycles a day, control the DO concentration in the reactor to be 0.5mg/L , 1mg/L , 1.5mg/L respectively, 2mg/L , 2.5mg/L , each group of DO concentration runs stably for 7 days, and each water inlet and outlet indicators are checked regularly every day to investigate the nitrosation situation under different DO concentrations. See attached table 6 for test data. Test results are shown in Figure 6 and Figure 7.

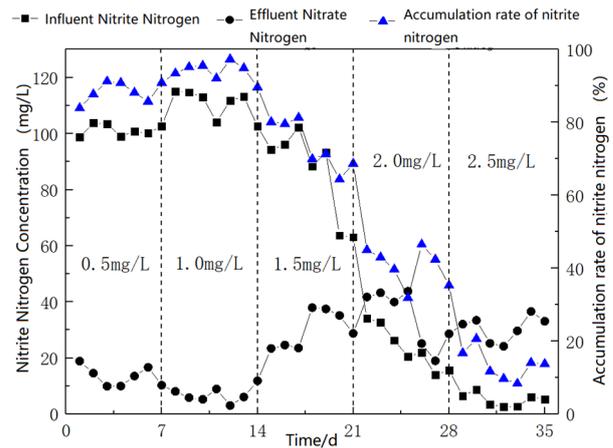


Fig6. The effect of DO on the removal effect of $\text{NH}_4^+\text{-N}$

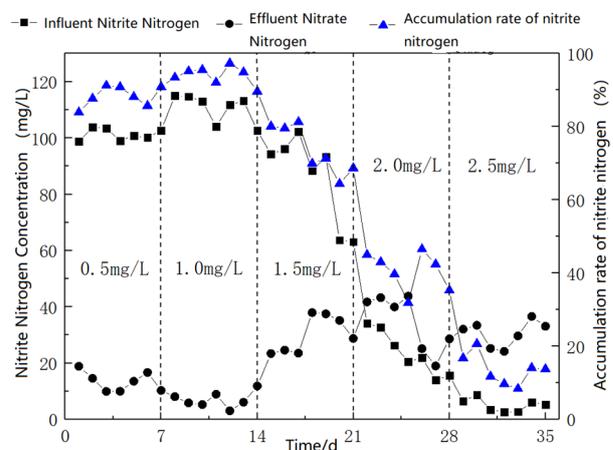


Fig7. The influence of DO on the cumulative effect of $\text{NO}_2^-\text{-N}$

It can be seen from Figure 6 that when the concentration of DO increases, the removal effect of $\text{NH}_4^+\text{-N}$ in the reactor is not significantly affected. Under these 5 different gradient concentrations, the average removal rates of $\text{NH}_4^+\text{-N}$ are 88.48% and 91.60% respectively, 84.21%, 94.66% and 92.27%, have always maintained a high level. Every time the DO concentration increases, the effluent $\text{NH}_4^+\text{-N}$ concentration changes little. The effluent $\text{NH}_4^+\text{-N}$ concentration is stable at about $12\text{mg}\cdot\text{L}^{-1}$ within 35 days, and the effluent quality is good.

As shown in Figure 7, when the DO concentration in the reactor is maintained at $0.5\text{mg}\cdot\text{L}^{-1}$ and $1.0\text{mg}\cdot\text{L}^{-1}$, the average concentration of $\text{NO}_2^-\text{-N}$ in the effluent is $105.95\text{mg}\cdot\text{L}^{-1}$, increasing the DO concentration to $1.5\text{mg}\cdot\text{L}^{-1}$, the nitrification in the reactor is weakened. When the DO concentration is controlled to $2.0\text{mg}\cdot\text{L}^{-1}$, the $\text{NO}_2^-\text{-N}$ accumulation effect will be further deteriorated, and the $\text{NO}_2^-\text{-N}$ concentration in the effluent will drop significantly. When $\text{DO}=2.5\text{mg}\cdot\text{L}^{-1}$, there is almost no accumulation of $\text{NO}_2^-\text{-N}$ in the reactor, but the concentration of $\text{NO}_3^-\text{-N}$ in the effluent has not been further increased and maintained at about $30\text{mg}\cdot\text{L}^{-1}$. The oxygen environment promotes the denitrification reaction, and a large amount of nitrogen is decomposed into N_2 and discharged from the reactor.

The test results show that the concentration of DO has a great influence on the nitrification reaction. The system carries out the whole nitrification and denitrification

reaction in a high dissolved oxygen environment, and nitrogen is more in the form of N_2 . In a low dissolved oxygen environment, it is conducive to the accumulation of NO_2^- -N, so that the oxidation process in the system stays in the nitrosation stage.

However, a too low DO concentration will cause a large number of filamentous bacteria to multiply. Taking into account comprehensively, the nitrosation effect is best when the DO concentration is controlled at $1.0 \text{ mg}\cdot\text{L}^{-1}$.

5 Conclusion

The experiment investigated the influence of temperature, pH and DO factors on the nitrosation performance of the reactor by studying the SBBR reactor with sodium chlorate inhibitor, and determined the optimal reaction conditions for each factor. The test results showed :

Temperature is an important factor affecting the nitrosation reaction. When the temperature range is around 30°C , the nitrosation process is the best; the pH value has an important influence on the nitrosation reaction. Controlling the pH between 7.5 and 8.0 is beneficial to the realization of an alkaline environment. Nitrosation reaction: Among them, DO concentration has the greatest influence on nitrosation reaction. When DO concentration is controlled at $1.0 \text{ mg}\cdot\text{L}^{-1}$, nitrosation is the best.

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